Advances in PNNL's Mixed Acid Redox Flow Battery Stack

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Topics

- ► FY 14 Objectives and Goals
- Background
- ▶ Nafion® membrane thickness development.
- Low cost interdigitated flow design
- ▶ 4 KW stack
- Conclusion and Future Work

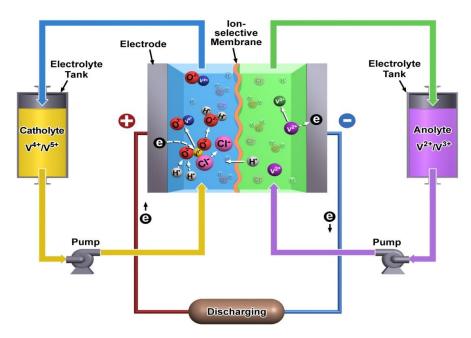


FY14 Redox Objectives and Goal

- Operate at 240 mA/cm² with improved stack energy efficiency and lower stack pressure drop.
- Greater stack efficiency
 - Use of 212/211 membrane versus 115.
- Greater system efficiency
 - Use of interdigitated flow field
- Understand influence of temperature on stack efficiency



Vanadium Mixed Acid Electrolyte



Catholyte:
$$VO^{2+} + Cl^{-} + H_2O - e$$

Charge
Discharge
 $VO_2Cl + 2H^+$
 $E_{co} = 1.0 \text{ V}$

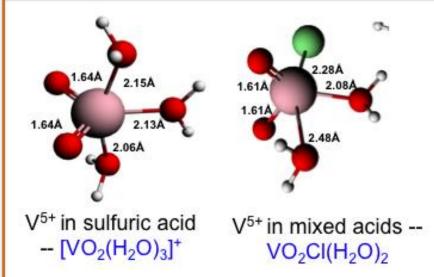
Anolyte: $V^{3+} + e$

Charge
Discharge
 V^{2+}
 $E_{a0} = -0.25$

Overall: $VO^{2+} + Cl^{-} + H_2O + V^{3+}$

Charge
Discharge
 $VO_2Cl + 2H^+ + V^{2+}$
 $E_{0} = 1.25 \text{ V}$

- Power and Energy are separate enabling greater flexibility and safety.
- Suitable for wide range of applications 10's
 MW to ~ 5 kw
- Wide range of chemistries available.
- Low energy density ~ 30 Whr/kg

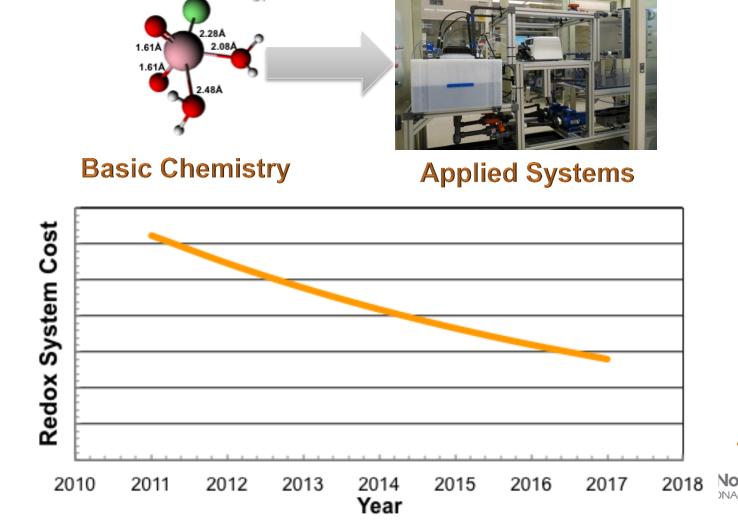


- > 70% increase in capacity
 - V²⁺, V³⁺, V⁴⁺, V⁵⁺ stable >2.8M, in SO²⁻ and Cl⁻ mixed solutions
- 80% increase in operating temperature window.
 - -5 50°C



Redox Flow Battery Objectives

Develop the technologies, tools, and system understanding required to move the mixed acid electrolyte chemistry from basic chemistry to cost effective system solution.



FY14 Stack Performance (Nafion® 115, 212 and 211)



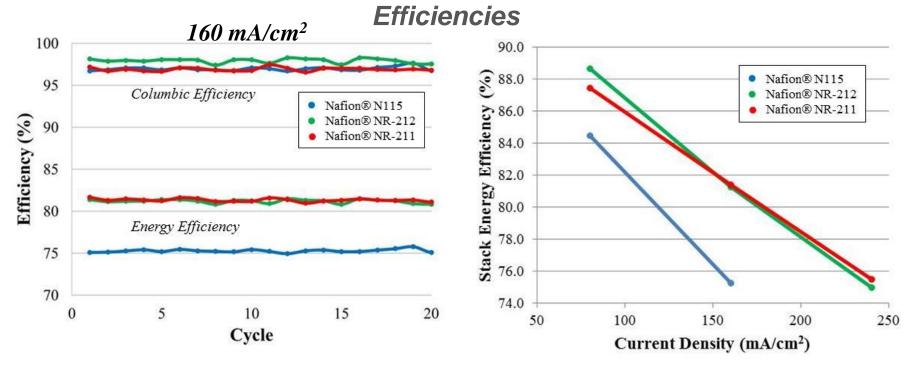
Test Parameters

- 780 cm²
- 3 cell stacks
- 15-85% SOC
- Mixed acid electrolyte
 - 2M V, 2M S, 2M Cl
- Nafion® membrane
 - 115 (~ 5 mil)
 - 212 (~ 2 mil)
 - 211 (~1 mil)
- *j* = 160 and 240 mA/cm2
- Flow through design

VRFB System



FY14 Stack Performance (Nafion® 115, 212 and 211)

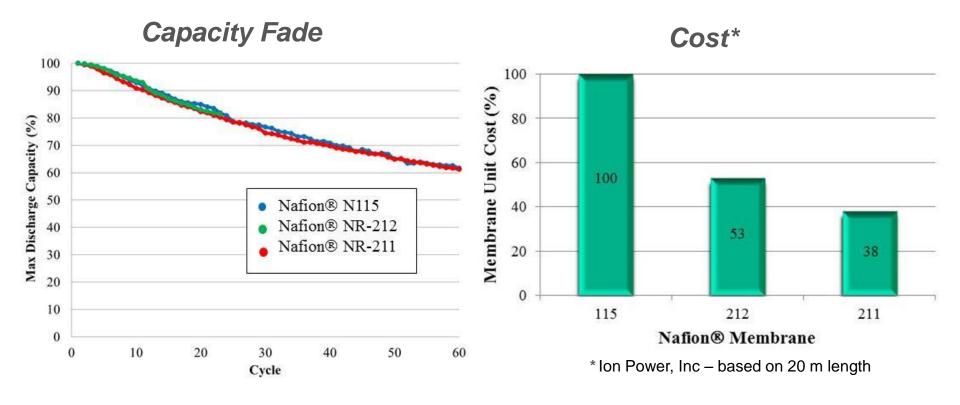


@Flow Rate = 6 lpm (400 cc/min/cell)

| | Columbic | Voltage | Energy | Discharge | Discharge | Pressure |
|------------------------|----------------|----------------|----------------|---------------|-----------|----------|
| | Efficiency (%) | Efficiency (%) | Efficiency (%) | Capacity (Ah) | Temp (°C) | (psi) |
| 160 mA/cm ² | | | | | | |
| Nafion® 115 | 96.9 | 77.7 | 75.3 | 18.2 | 39.9 | 6.5 |
| Nafion® 212 | 97.9 | 82.9 | 81.2 | 19.2 | 39.9 | 6.9 |
| Nafion® 211 | 96.9 | 84.0 | 81.4 | 20.1 | 38.8 | 6.9 |
| 240 mA/cm ² | | | | | | |
| Nafion® 212 | 98.0 | 76.5 | 75.0 | 16.7 | 44.6 | 6.1 |
| Nafion® 211 | 97.0 | 77.8 | 75.5 | 18.1 | 45.5 | 5.9 |

LABORATORY

FY14 Stack Performance (Nafion® 115, 212 and 211)

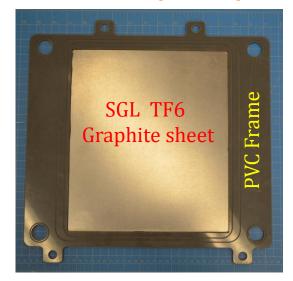


- Substitution of Nafion® 212 and 211 for 115 in 3-cell stack leads to
 - ~5 10% increase in Energy Efficiency (≥ 160 mA/cm²)
 - Similar capacity fade
 - Cost reduction
- Nafion® 211 more difficult to handle

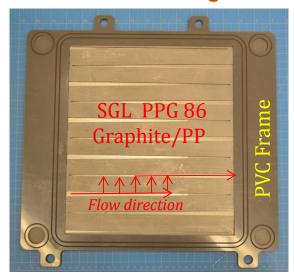


FY14 Stack Performance (Low Cost IDD Flow Design)

Flow Through Design



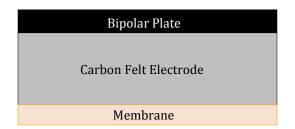
IDD Flow Design



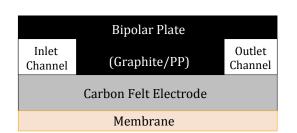
Low Cost IDD Flow Design



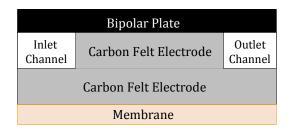
(FTD)



(IDD 1)

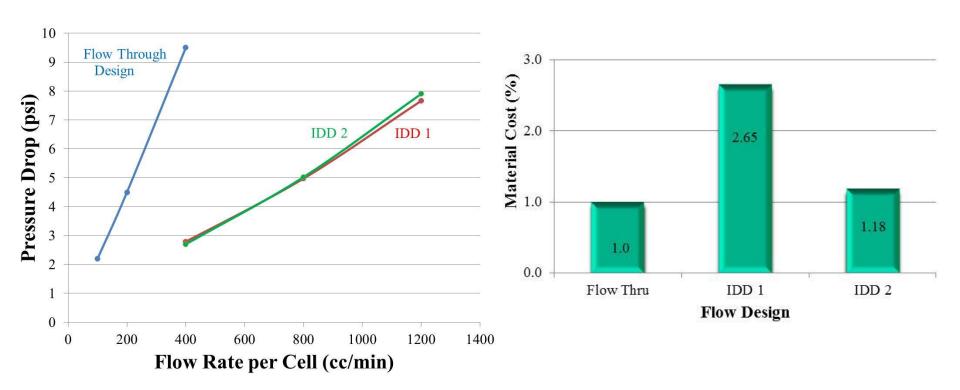


(IDD 2)



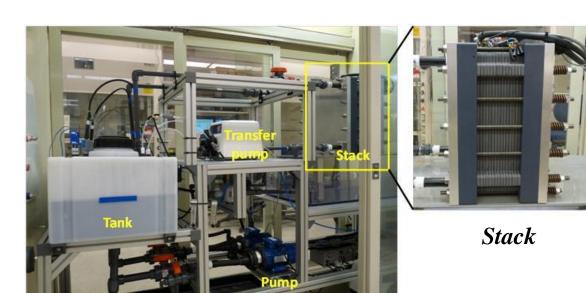


FY14 Stack Performance (Low Cost IDD Flow Design)



- ► Higher flow rates with IDD 1 and IDD 2
- ► IDD 1 approximately 3X material cost
- Sealing issues with IDD 1





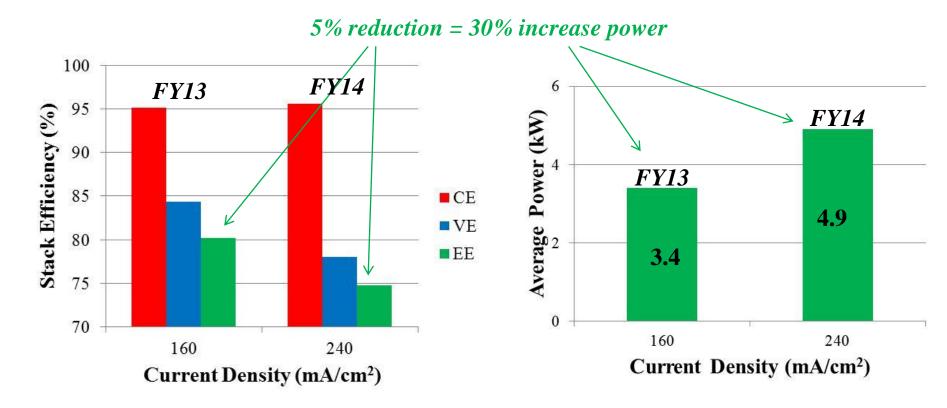
VRFB System

Test Parameters

- 780 cm²
- 20 cell stack
- 15-85% SOC
- Mixed acid electrolyte
 - 2M V, 2M S, 2M Cl
- Nafion® membrane
 - 212 (~ 2 mil)
 - j = 160 and 240 mA/cm²
- Low cost interdigitated flow design
- 4 KW stack
- Chillers to control temperature



20 Cell Stack − 50 °C, 800 cc/min/cell, Nafion ® 212

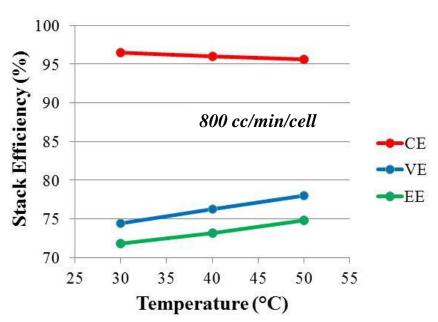


- ▶ 5% reduction in Stack Energy Efficiency
- 30% increase in Power

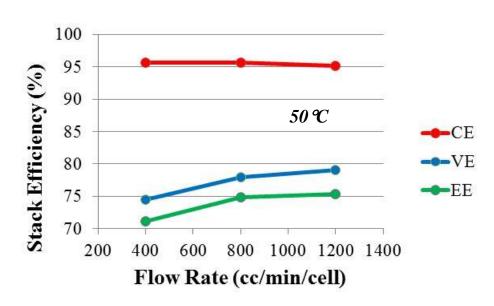


20 Cell Stack - 240 mA/cm² Nafion @ 212





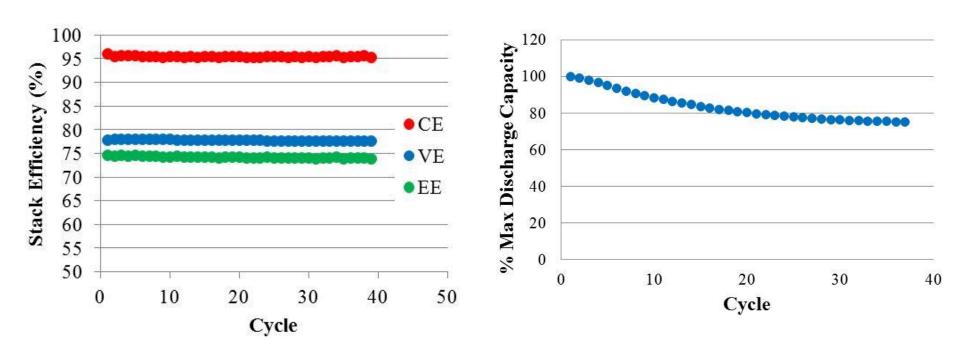
Efficiency vs Flow Rate



Pacific Northwest

Flow rate and temperature both improve stack energy efficiency

20 Cell Stack $-50 \, \text{C}$, 800 cc/min/cell, Nafion @ 212



Stable performance for mixed acid electrolyte observe over a broad range of temperatures and flow rates



Summary/Conclusions

- Substitution of Nafion® 212 or 211 for 115 in 3-cell stack leads to
 - ~5 10% increase in Energy Efficiency (≥ 160 mA/cm²)
 - ~ 50% cost reduction
- Low cost IDD had similar performance to original IDD but has a substantial reduction in material cost
- The 4kW class 20 cell stack operated at 240 mA/cm² resulted in
 - ~ 30% increase in power
 - 5% reduction in energy efficiency (75%)
 - Stable performance over a range of temperatures and flow rates using the mixed acid electrolyte

Acknowledgements

□ DOE-OE Energy Storage Program, Dr. Imre Gyuk

